(Exhibit 1)

DECLARATION OF TRANSLATOR

I, Kenji KABUKI, c/o the Inoue & Associates of 3rd Floor, Akasaka Habitation Building, 3-5, Akasaka 1-chome, Minato-ku, Tokyo, Japan do solemnly and sincerely declare that I am conversant with the Japanese and English languages and that I have executed with the best of my ability this partial translation into English of D1, i.e., JP-A-2002-219362, and believe that the translation is true and correct.

May 20, 2008
(Date)

Kenji KABUKI

10/541,393

Exhibit 1

Partial English translation of D1, i.e., JP-A-2002-219362

(1) Front page (page 1), upper portion:

(12) Laid-Open Patent Gazette (A)

(11) Unexamined Japanese Patent Application Laid-Open Specification No. 2002-219362

(22) Filing date: January 24, 2001

(43) Laying-open date: August 6, 2002

(71) Applicant: Asahi Kasei Corporation

(54) [Title of the invention] Silica-supported catalyst having a low specific gravity

(2) Column 1 (page 2), lines 1 to 22:

[Scope of claims]

[Claim 1] A silica-supported catalyst for use in gaseous phase catalytic oxidation or ammoxidation of propane or

isobutane for producing an unsaturated carboxylic acid or an unsaturated nitrile,

said catalyst satisfying the following requirements (a), (b) and (c):

(a) said catalyst comprises a composition represented by the following formula (I):

$$Mo_1V_aSb_bNb_cZ_dO_n \qquad (I)$$

wherein:

Z is at least one element selected from the group consisting of W, Cr, Ti, Al, Ta, Zr, Hf, Mn, Re, Fe, Ru, Co, Rh, Ni, Pd, Pt, Cu, Ag, Zn, B, Ga, In, Ge, Sn, P, Pb, Bi, Y, rare earth elements and alkaline earth metals; and

a, b, c, d, and n are, respectively, the atomic ratios of vanadium (V), antimony (Sb), niobium (Nb), Z and oxygen (O), relative to molybdenum (Mo),

wherein:

$0.1 \leq a \leq 1$,

$0.01 \leq b \leq 0.6$,

$0.01 \leq c \leq 0.3$,

$0 \leq d \leq 1$, and

n is a number determined by and consistent with the oxidation states of the metal ele-

ments present,

(b) the oxide represented by the formula (I) is supported on a silica carrier, said silica carrier being present in an amount of from 20 to 60 % by weight, and

(c) said catalyst has a pore volume of 0.15 cm^3/g or more.

(3) Column 18 (page 10), line 27 to columns 19 and 20 (page 11), lines 1 to 39:

[0065]

[Table 1]

	Composition of catalyst					Catalyst preparation conditions	Physical properties of catalyst			Ammoxidation of propane		
	Mo	V	Sb	Nb	SiO_2 (wt%)	....	Pore volume (cm3/g)	Bulk density (g/cm3)	spherical index	contact time (S)	propane conversion (%)	acrylonitrile selectivity (%)
Example 1	1	0.3	0.23	0.07	....	.....	.....	.....	.....	...	48.6	63.8
Example 2	1	0.3	0.23	0.07	....	.....	.....	.....	.....	...	50.1	63.0
Comparative Example 1	1	0.3	0.23	0.07	....	.....	.....	.....	.....	...	48.5	63.9
Comparative Example 2	1	0.3	0.23	0.07	....	.....	.....	.....	.....	...	48.6	63.9
Example 3	1	0.23	0.25	0.09	....	.....	.....	.....	.....	...	48.0	67.8
Example 4	1	0.23	0.25	0.09	....	.....	.....	.....	.....	...	49.3	67.7
Comparative Example 3	1	0.23	0.25	0.09	....	.....	.....	.....	.....	...	48.2	67.8
Example 5	1	0.3	0.22	0.07	....	.....	.....	.....	.....	...	48.0	63.2
Comparative Example 4	1	0.3	0.22	0.07	....	.....	.....	.....	.....	...	48.3	63.2

(4) Column 19 (page 11), lines 40 to 45:

[0066]

[Effect of the invention] The silica-supported catalyst of the present invention exhibits a large volume while maintaining the reaction results at the same level as in the case of the conventional silica-supported catalysts. Therefore, the catalyst exhibits a high flowability and hence a high efficiency of gas-catalyst contact, thereby facilitating the operation of a fluidized bed reactor.